

TOWNE

378.748

POS 1899.5





THESIS  
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WHIP  
BENT.

Heat Losses  
and  
Efficiencies  
of  
Otto Gas Engine.

A. St. S. Cantlin:  
Widney Hilborn.

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378.748

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Test of a One-Third Horse  
Power Otto Gas Engine.

The following thesis is an account of a test on a one-third horse power Otto Gas Engine, manufactured by the Otto Gas Engine Company, 33<sup>rd</sup> and Walnut Streets, Philadelphia, to determine the heat distribution, efficiencies and indicated and brake horse powers.

The engine is part of the equipment of the mechanical laboratory of the University of Pennsylvania.

Two half hour - thirty minute - runs were made with the conditions as nearly identical as possible and they were taken together and worked up as one

1605  
C. A. H. Smith

4 June '48. Ser. g. Univ.



test.

In the following description, the letters and numbers refer to the photograph of the engine and the apparatus used during the test on page 14a:

The engine consists of a vertical cylinder (16), 3 inches in diameter with a trunk piston packed with 5 metallic rings. The piston is connected to a cranked shaft (1) by the connecting rod (2) which has a 5 inch stroke.

On one end of the shaft is the fly-wheel (10), two feet in diameter, and on the other a gear wheel, which gears into another wheel having twice the number of teeth. These gear wheels are enclosed in the cast iron case (9).







On the shaft of the second gear wheel is an eccentric which operates the rod (22). This in turn operates the exhaust valve (u) and the governor (v). The governor controls the admission of the gas to the chamber (v) where it is stored before being admitted to the cylinder. The gas together with the air is admitted to the cylinder by the disc valve (w) which is raised by suction every fourth stroke of the piston. This valve has a number of holes in its seat which communicate with the chamber (v). Underneath, the valve is in communication with the air space between the bottom wall of the cylinder and the base of





the engine. When the valve is raised a mixture of air and gas is admitted which depends on the relative area through the holes and under the valve. The valve is held to its seat by a spring.

The governor consists of a round, threaded weight (r) on the end of a lever having a screw thread and a lock nut so the position of the weight can be changed. Its fulcrum is at (q) and the further end of the lever is held down by the spring (o). The pivot at (q) is part of the valve rod (22). Projecting downward from the fulcrum is a small rod (p) which is cast in one piece with the lever and which car-





ness a hook at its lower end.

When the rod (p) hangs vertical, the hook on the rod engages with a projection on the stem of the valve at (t) being held to its place by the spring (o).

When the rod (22) is lifted the governor goes with it and the valve is raised admitting gas to the chamber (V). If the speed gets too fast the inertia of the weight overcomes the pull of the spring and causes the hook to miss the projection. The valve is not raised and no gas admitted. Consequently there is no explosion and the speed is reduced. The speed can be regulated by the position of the weight (r) on the





lever.

The gas is drawn from the main and passes through the meter (d), the equalizing bag (f) and the tap (g). The latter is supplied with a graduated disc and pointer.

The gas for the Bunsen burner enclosed in the cast iron cylinder (h) is drawn through the meter (e) and the regulating cock (23). This cylinder is lined with asbestos and an iron tube of small diameter, closed at the top, extends up the centre. The fire plays round this tube and keeps it red hot. The charge is compressed into this tube and exploded.

The air used is admitted





to the space below the cylinder wall through the pipe (6) and also through small holes in the bedplate.

The exhaust gases pass out through the exhaust valve (u) and the pipes (v) and (18) into the outside air.

A water jacket surrounds the cylinder, the water entering at the bottom and exhausting at the top through pipes at the back which cannot be seen in the picture. By means of pet cocks the water can be exhausted through the floor or discharged into collecting buckets.

The engine works in what is known as an 'Otto cycle' and takes four strokes to complete a cycle. On the



first upward stroke the mixture is drawn into the cylinder; on the downward it is compressed and ignited as the engine reaches the dead point; on the third expansion takes place and on the fourth, the exhaust.

The suction valve takes care of itself, while by means of the second gear wheel in the case (y) having twice the number of teeth on the first the other valves are opened every fourth stroke instead of every second.

Several precautions are necessary. All the valves must be kept clean and fit their seats truly or the engine will not run.

If the compression is not





good there will not be any explosion. The valve (w) must also be adjusted so that it is not raised too easily or too much. The supply of gas must also be regulated to suit the load, as for any given load there are certain limits in each direction for the ratio of air to gas and if these limits are passed there is no explosion and the engine stops. The ignition tube must also be kept hot. On starting the flywheel must be spun comparatively fast before an explosion will occur.





## Instruments.

The following apparatus was used:

The brake for determining the brake horsepower consisted of a strong cord (8) held in position by three wooden guides (9). On one end is hung a weight while to the other is attached the spring balance (7) which was held by a hook (19) in the floor.

The cards for the indicated horse power were taken with a Thomson Indicator (3) having a piston with an area of one quarter square inch and a larger one of one half a square inch. It was attached to the pipe (24) in connection with the lower



part of the cylinder. Communication was through a cock (2) on the pipe. The larger cylinder was used.

To get the required motion for the drum (3), a string (12) was fastened to a pin projecting from the hub of the fly wheel. This string was strong and was tied so it would not tighten and wrap up on the pin. It carried a loop at the lower end. Another string (25) was wound around the drum and had a hook on its free end. When the engine was running the string (12) was flung out by centrifugal force and could be caught in the hand.

The hook of (25) was then placed in the loop of string (12) and the desired motion given to the drum (3).





For the number of revolutions the counter (m) was fastened to a wooden frame and held firmly by being wedged under the piping. The iron rod (21) was clamped on the rod (22) and a wire at its outer end worked the counter. The counter was pulled back by a spring not shown in the picture. The number of revolutions is found by multiplying the reading of (m) by two since the rod (22) moves up and down once in every two revolutions.

For the number of explosions the counter (n) was attached to the valve (4) which supplies gas. When gas was admitted the valve was raised and this worked the counter. The gas for combustion was





measured by the meter (d) and gas for ignition by the meter (e).

The temperature of the incoming gas was measured by the thermometer (a) placed in a thermometer well (b) in the supply pipe.

The temperature of the exhaust gases was determined by the thermometer (i) also in a thermometer well.

A Bristol Recording Gauge - not shown in picture - in communication with (26) recorded the gas pressure in inches of water.

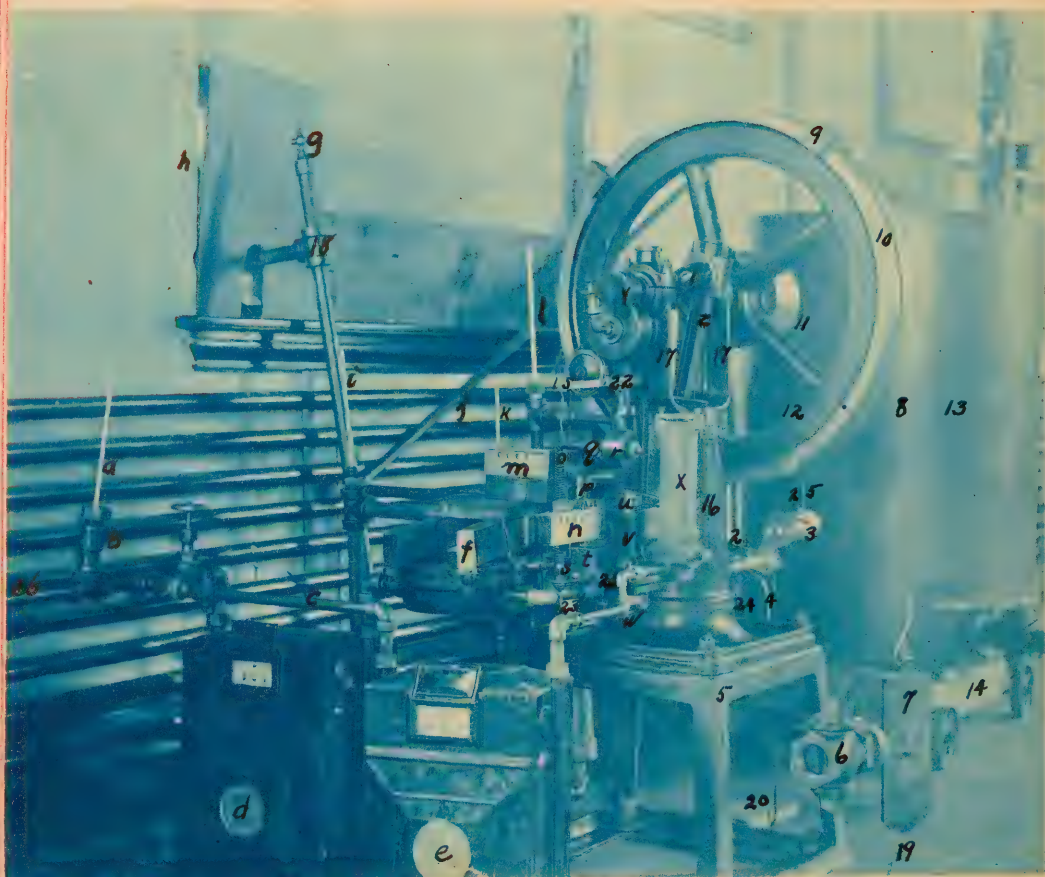
The temperature of the room was measured by the thermometer (h)

In order to keep the cylinder cool a certain amount of water, regulated by the outlet cock, was allowed to flow through the jacket and was caught in buckets.



and weighed, the buckets being weighed full and empty. The thermometers (H) and (L) placed in thermometer wells on the pipes measure the temperatures of the water at inflow and outflow respectively. The flow was regulated so the rise in temperature of the water was about constant during the test.

The clearance volume was determined by removing the piston and filling the cylinder up to a certain mark with water. The weight of this water was determined by taking the difference in weight of a bucket of water before the water to fill the cylinder was taken out, and after. The difference gives the weight and from this the





volume up to the mark was determined by finding the weight of a known volume of the water in a 200 c.c. bottles. By determining the volume from the mark to the bottom of the piston when at the bottom of its stroke and subtracting this from the first volume gives the clearance volume.

The circumference of the fly wheel was determined directly by wrapping a tape measure around it.

### Calibration of Instruments.

The gas meters were calibrated by connecting them in series to the top of a stand pipe filled with water. The water was then run out into a tank



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and weighed and the volume calculated. The readings of the meters before and after were taken and from these the readings of the meters for each cubic foot determined.

The indicator spring was calibrated by placing it on a siphon on a steam line and throttling the steam. readings being taken ascending and descending when the pressure was indicated by the steam gauge on the siphon on the steam line. The accuracy of the gauge was then tested with the Crosby Gauge Tester. The spring used was marked 100 lbs.

The spring balance was calibrated by hanging standard weights on it and was found correct.



As the 'Wristol Recording Gauge' read above the atmosphere, one leg of a manometer was opened to the atmosphere and the other connected to a glass Y tube by means of a rubber tube. One other leg of the Y was connected to the gauge and by blowing into the third leg, any pressure desired above the atmosphere could be measured on the manometer and compared to the gauge. The gauge was found correct. The humidity was found from the report of the U. S. Weather Bureau for Philadelphia.





## Symbols.

$H_g$  = barometric height in inches of mercury

$P_g$  = barometric pressure in pounds per square foot.  $P_g = H_g \times 4.888 \times 144$

$P_a$  = press. of air =  $P_g - P_{aw}$

$P_{aw}$  = vapor press. in air, assuming air saturated.

$h$  = % humidity

$P'_{aw}$  = vapor pressure in air at observed degree of saturation.  $P'_{aw} = h P_{aw}$

$w_{aw}$  = wt. of moisture in 1 cu. ft. of saturated air

$w_{aw}$  = " " " " " " " " air, when humidity is  $h$  %.  $w_{aw} = h w_{aw}$

$T_a$  = absolute temp. of air

$b_a$  = per centage of air by weight in mixture of gas and air

$b_g$  = per centage of gas by weight in mixture of gas and air.  $b_g$  = air, or  $b_g$  = gas.



$M_a$  = total mass of air =  $\frac{v_a}{v_g} M_g$

$M_a'$  = mass of air for explosions

$V_a$  = total vol. of air per hour =  $\frac{M_a R_a T_a}{P_a}$

$R_a$  = constant for air

$V_a'$  = vol. of air per hour for explosions

$v_a$  = vol. of air per minute =  $\frac{V_a}{60}$

$v_a'$  = vol. of air per min. for explosions =  $\frac{V_a'}{60}$

$T_{am}$  = temp. of vapor corresponding to pressure  $P_{am}$

$m_a$  = mass of air per explosion =  $\frac{v_a}{T_g} w_g$

$H_g$  = press. in gas main in inches of water

$P_g$  = press. in lbs. per sq. ft. corresponding to

$$H_g = \frac{62.4 \times 2.2}{12} \times H_g$$

$P_{gw}$  = press. of moisture in gas, assuming gas saturated at temp. of gas in main

$T_g$  = abs. temp. of gas in main

$w_{am}$  = weight of moisture in cu ft of saturated gas

$v_g$  = vol. of gas per min. at initial condition

$v_g'$  = vol. of gas per min. at initial condition

$P_g$  = press. of gas =  $P_a + P_g - P_{am}$





$V_1$  = vol. of gas per hour in non-ignition.

$V_2$  = vol. of gas per hour for ignition.

$V_{10}$  = vol. of gas per hour without ignition.

$R_g$  = correction for gas

$N_r$  = revolutions per min.

$N_a$  = no. of possible admissions per min. =  $\frac{N_r}{2}$

$N_e$  = no. of explosions per min.

$T_g$  = vol. temp. of exhaust gas.

$T_e$  = temp.  $T$  of exhaust after.

$v_a$  = vol. of gas per explosion =  $\frac{V_2}{N_e}$

$v_{gs}$  = specific vol. of gas =  $\frac{R_g T_g}{P_g}$

$w_a$  = vol. of gas per explosion =  $\frac{v_a}{v_{gs}}$

$w_{eH}$  = vol. of moisture in exhaust per min.

$P_e$  = press. of exhaust gas  $c = P - P_{em}$

$P_{em}$  = press. of moisture in exhaust add.

$W_1$  = vol. of inlet water per min.

$T_1$  = temp. of water entering

$T_2$  = temp. of water leaving

$q$  = heat of fusion



$r$  = heat of vaporization

$c_v$  = spec. heat at constant volume

$c_p$  = spec. heat at constant pressure

$H$  = wt. of hydrogen in liq. & gas.

$P_m$  = constant for vapor of water at low pressures

$T_m$  = temp. corresponding to pressure  $P_m$ .

$M_w$  = mass of water per hour

$L$  = length of rope in feet

$a$  = area of piston

$P$  = mean effective pressure =  $\frac{A}{L}$ .

$A$  = area of card

$C_a$  = calorific value of the fuel gas

$W_1$  = wt on scale side of rope brake

$W_2$  = wt on opposite side

$W_1 - W_2 = W$  = net pull on rope brake

$H_c$  = heat of combustion, per min.

$H_a$  = heat brought in in air per min.

$H_{am}$  = heat brought in in moist. of air per min.



$H_f$  = heat brought in in fuel per min.

$H_{fm}$  = heat brought in in moist. of fuel per min.

$H_e$  = heat in exhaust gas per min.

$H_{em}$  = heat in moist. of exhaust gas per min.

$H'_e$  = heat carried off by jacket water per min.

$I_a$  = indicated work in heat units

$H_r$  = heat lost by radiation.

$e$  = mechanical efficiency

$E'$  = hyp. efficiency

$E''$  = actual efficiency





Formulae.

$P$  &  $T$  = press. and temp. in cylinder.

$$\text{vol. of gas} = \frac{M_g R_g T}{P}$$

$$\text{vol. of air for explosion} = \frac{M_a R_a T}{P}$$

$$\frac{\frac{M_g R_g T}{P} + \frac{M_a R_a T}{P}}{N_e} = \frac{\frac{(M_a - M_a') R_a T}{P}}{N_e - N_e}$$

$$M_a' = M_a \frac{N_e}{N_a} - M_g \frac{R_g}{R_a} \cdot \frac{N_e - N_e}{N_a} \quad (1)$$

$$H_c = C_a \times w_{ga} \times N_e \quad (2)$$

$$H_a = c_p \frac{M_a}{60} \times (T_a - T_{32}) \quad (3)$$

$$H_{au} = w_{au} \left[ q_{au} + r_{au} + 48(T_a - T_{au}) \right] N_a \quad (4)$$

$$H_g = c_p \frac{M_g}{60} (T_g - T_{32}) \quad (5)$$

$$H_{gu} = w_{gu} (q_{gu} + r_{gu}) \frac{V_g}{60} = w_{gu} \times r_{gu} \times \frac{V_g}{60} \quad (6)$$

$$H_e = c_p (T_e - T_{32}) \frac{M_g + M_a}{60} \quad (7)$$

$$H_{eu} = w_{eu} [q_{eu} + r_{eu} + 48(T_e - T_{eu})] \quad (8)$$

$$H_f = \frac{M_u}{60} (q_1 - q_2) = M_f (q_1 - q_2) \quad (9)$$

$$H_i = \frac{(I. H. P.) \times 33000}{778} \quad (10)$$

$$H_r = (H_c + H_a + H_{au} + H_g + H_{gu}) - (H_e + H_{eu} + H_f + H_i) \quad (11)$$

$$\frac{P_e N_e}{P_{eu} N_e} = \frac{M_e R_e T_e}{w_{eu} R_u T_e} \quad P_e - P_{eu} = P_e$$



$$P_e = \frac{M_e K_e}{W_{em} R_m} P_{em} = \frac{M_e K_e}{W_{em} R_m} (P_o - P_e)$$

$$\left(1 + \frac{M_e R_e}{w_e R_w}\right) P_e = \frac{M_e R_e}{w_e R_w} P_b$$

$$P_{ew} = P_e \frac{w_{ew} R_m}{M_e R_e} = P_e \frac{M_e R_e}{w_{ew} R_m (1 + \frac{M_e R_e}{w_{ew} R_m})} \cdot \frac{w_{ew} R_m}{M_e R_e}$$

$$P_{em} = \frac{P_e}{1 + \frac{M_e R_e}{w_{em} R_{em}}} \quad (12.)$$

$$w_{em} = 9H \frac{Mg}{68} + w_{am} \tau_a + u_{gm} \tau_g \quad (13)$$

$$I.H.P = \frac{P L a N_c}{33000} \quad (14)$$

$$B.H.P = \frac{\pi r N r W}{33000} \quad (15)$$

Vol. of gas per I. H. <sup>per hr</sup>  $\times$  moist  $\times$   $\frac{V_g}{V_g + V_a}$  (16)

" " " " " with " =  $\frac{V_1 + V_2}{I.H.P.}$  (97)

" " " " B. H. I. <sup>her</sup> without " =  $\frac{V_2}{B. H. P.} (18)$

" " " " " with " =  $\frac{V_2 + V_1}{B.H.P.}$  (19)

$$e = \frac{B.H.P.}{I.H.P.} \quad (20)$$

$$E' = 1 - \frac{T_3}{T_4}$$

$$\frac{T_2}{T_4} = \left(\frac{v_4}{v_2}\right)^{\gamma-1} \quad E = 1 - \left(\frac{v_4}{v_2}\right)^{\gamma-1} \quad (21)$$

$$E'' = \frac{H_i}{H_e}$$

$$F_2 = \frac{F_1}{E}$$

(23)





# *Tables.*



# Table 1.

## Counters.

Time.	Rev.	Explosion.
12.37	4919	7822
12.43	5920	8572
12.50	7280	9700
12.56	8430	10720
1.01	9440	11575
1.07	10650	12600
2.25	9100	6090
2.31	9945	6845
2.36	10585	7475
2.41	11205	8205
2.46	11800	8700
2.51	12480	9240
2.56	13130	9770



# Table 2.

## Temperatures.

Time.	Gas.		Jacket Water.		Air.
	Inlet	Exhaust	Inlet	Exhaust	
12.37	84	363	80	110	84
12.43	84	387	78	105.5	85
12.50	84	430	79	109.	85
12.56	84	461	77.5	98	85
1.01	84	474	78	105.5	85
1.07	84	479	79	107	85
2.25	86	404	80	108.5	87
2.31	86	419	83.5	113.	87
2.36	86	420	82	106.5	87
2.41	86	428	79.5	105.5	87
2.46	86	428	81	104.	87
2.51	86	429	80	106.	87
2.56	86	426	83.5	104.5	87





# Table 3.

## Jacket Water.

Time.	No. Bucket	Empty. lbs. oz.		Full. lbs. oz.	
1h 37.00	1	2	14 $\frac{1}{4}$	22	15 $\frac{1}{2}$
1h 44.10	2	2	11 $\frac{3}{4}$	20	15 $\frac{1}{2}$
1h 47.00	1	2	14 $\frac{1}{2}$	21	1
1h 51.10	2	2	11 $\frac{1}{2}$	23	13 $\frac{1}{4}$
1h 54.10	1	2	14 $\frac{1}{2}$	21	11 $\frac{1}{2}$
1h 57.30	2	2	11 $\frac{1}{2}$	21	00 $\frac{3}{4}$
1.04.30	1	2	14	12	11
1.07.00					
2.25.00	1	2	14 $\frac{3}{4}$	20	2 $\frac{1}{4}$
2.29.45	2	2	11 $\frac{3}{4}$	21	14 $\frac{1}{2}$
2.35.10	1	2	14 $\frac{1}{2}$	22	15 $\frac{1}{2}$
2.38.40	2	2	11 $\frac{1}{4}$	22	13 $\frac{3}{4}$
2.46.55	1	2	14 $\frac{3}{4}$	22	8 $\frac{1}{4}$
2.47.30	2	2	11 $\frac{3}{4}$	24	2
2.52.00	1	2	14 $\frac{1}{2}$	22	3 $\frac{1}{2}$
2.56.10					



# Table 4.

Meters - Gas.

Time	Cylinder	Time.	Ignition.
12.26.35	0	12.57.45	0
12.31.50	2	12.48.30	1
12.36.45	4	1.00.00	2
12.41.55	6	1.06.15	2.5
12.47.25	8	—	—
12.53.00	10	—	—
12.57.50	12	—	—
1.00.05	13	—	—
2.26.35	0	2.18.30	0
2.32.00	2	2.29.30	1
2.37.10	4	2.52.30	3.
2.42.25	6	—	—
2.47.30	8	—	—
2.52.30	10	—	—
2.57.20	12	—	—





# Table 5.

## Brake.

Time.	lbs.	oz.
12.57	2	15
12.43.	3	2
12.50	3	4
12.56.	3	8
1.07	3	10
1.07.	3	10
2.25	3	8
2.31	3	8
2.56.	3	12
2.41	3	12
2.56.	3	12
2.51.	4	0
2.56	4	0

Wt of poise -  $14\frac{1}{2}$  oz.

" " balance - 2 lbs.  $3\frac{1}{4}$  oz.



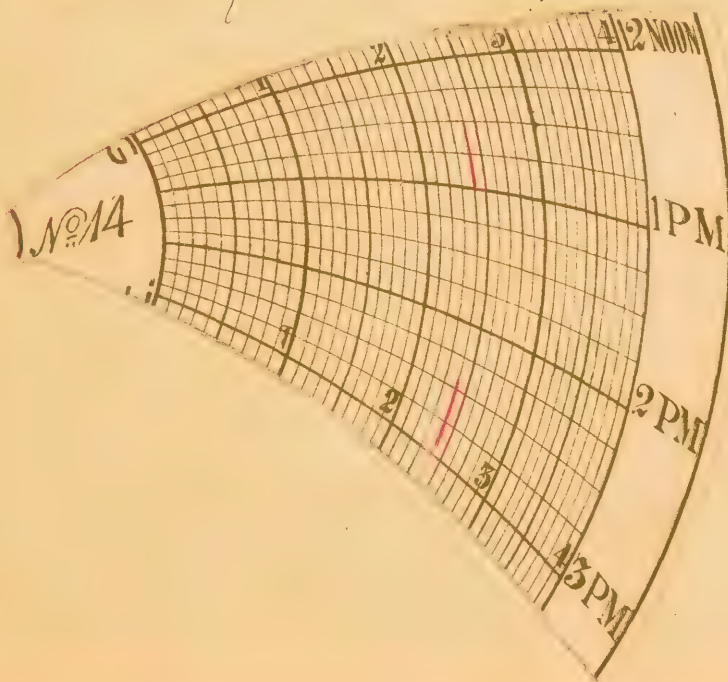
Additional Readings.

Calibration of Meters.

Cylinder meter 1 cu. ft. 1.177 cu. ft.  
 Gasometer 1 cu. ft. 2.001 cu. ft.

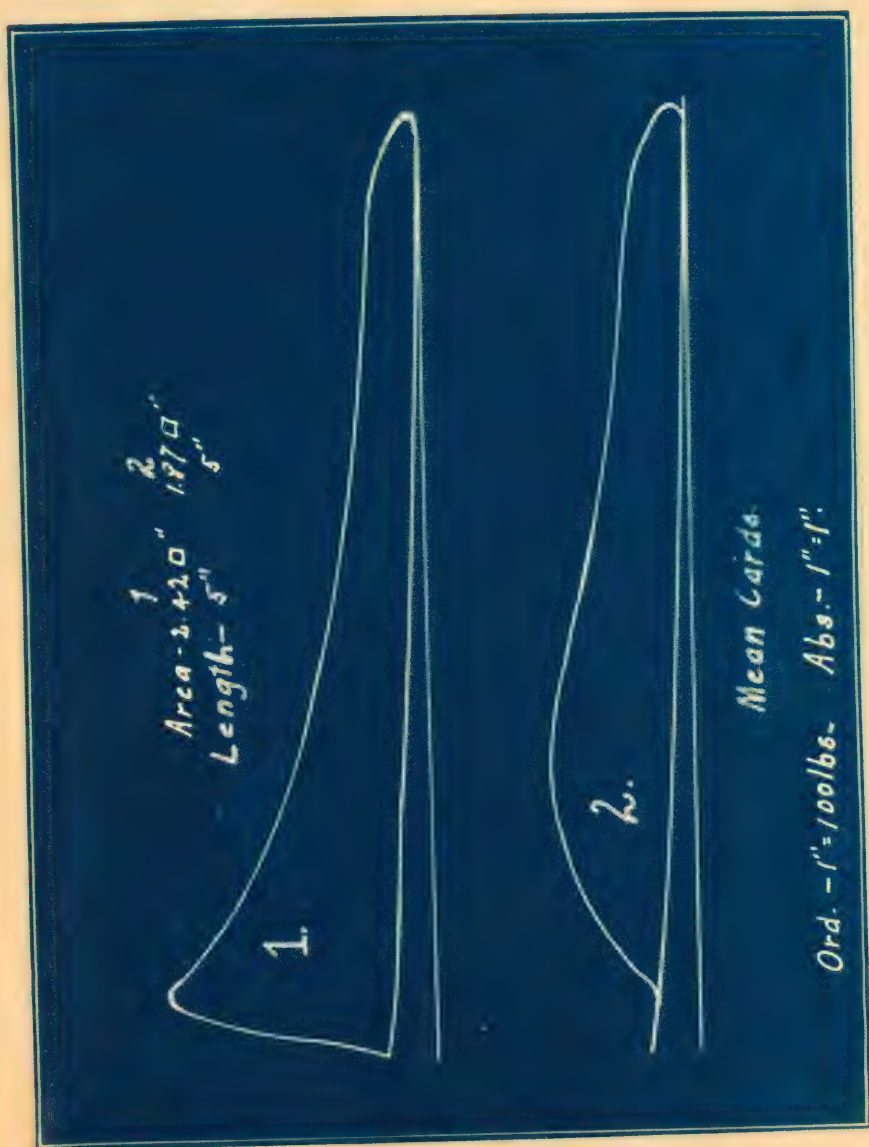
U. S. WEATHER BUREAU. Philadelphia. Monday, May 1, 1899.									
Time.....	Barometer.....	Temperature.....	Relative Humidity.....	Wind.		Rainfall.....	State of Weather.....		
				Direction	Velocity				
8 A. M.	30.11	61	83	S. W.	12	0	Pt. Cl'dy		
8 P. M.	30.00	74	59	S. W.	12	0	Pt. Cl'dy		

Bristol Recording Gauge.  
 Card from Gas Main.





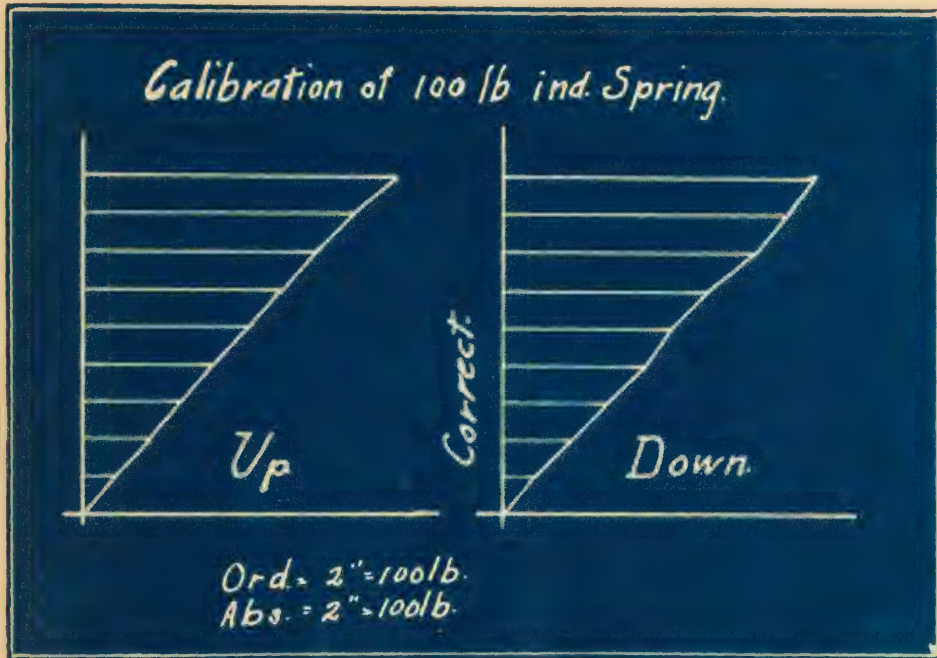
# Mean Cards.







## Indicator Spring Calibration Curve.



The Mean Cards above were constructed in the following manner: Each card had its base divided into 10 parts: In order for these parts to be equal parts of the stroke, the angularity



of the connecting rod and string.  
was allowed for by connecting  
up the indicator as in use and  
moving the piston equal parts  
of its stroke and a mark  
made with the indicator pencil  
on a paper on the drum and  
the cards correspondingly marked.  
The distances on the mean card  
were made equal and the  
corresponding pressures corrected  
according to the spring cali-  
bration.





## Test.

In starting the test the engine was run up to speed with the required load and run for about a quarter of an hour under the conditions of the test until the temperatures become steady. The test was started by a simultaneous reading of the revolution and explosion counters. Then the temperatures of the room, inlet and exhaust gases, and inlet and discharge jacket water and the reading of the brake were made in order and a card taken from the indicator. This series of operations was repeated every five minutes. One run



ute before the beginning of the test a bucket was placed under the jacket water outlet and as the buckets filled they were weighed and emptied. Two buckets were used and one minute before the end of the test the last bucket was removed and weighed, the water flowing at practically the same rate all the way through. The test was ended by taking a simultaneous reading of the revolution and explosion counters after which the temperatures and brake were read to fill out the readings, before the engine was stopped. at intervals during the



test samples of the fresh and exhaust gases were taken and were subsequently analyzed in a set of Hempel's apparatus.

The exhaust gas was drawn from the pipe (18) by a rubber tube attached above the cock (9) and the gas collected over water in a sealed bottle. By opening the cock (9) the gas was drawn out.

A similar arrangement on the gas main (26), not shown in the picture, allowed the fresh gas to be collected.

The time the two cubic foot hand of the combustion gas meter passed a mark just before the test, was noted and every time it again passed the mark was noted until after the end of the





test. From this the gas used during  
the test was computed.

In a similar manner every  
time the equation meter hand  
passed a one cubic foot mark,  
the time was noted.



# *Results.*



# Analyses of Gases.

## Philadelphia Illuminating Gas.

	% Vol.			% Wt.
$CO_2$ —	2.4	$\times 22 =$	52.7	6.70
$CO$ —	16.5	$\times 14 =$	230.5	29.30
$O$ —	.6	$\times 16 =$	9.6	1.22
$C_2H_4$ —	5.2	$\times 14 =$	72.8	9.89
$H$ —	31.7	$\times 1 =$	31.9	4.05
$C_4H_4$ —	37.1	$\times 8 =$	296.5	37.65
$N$ —	6.5	$\times 14 =$	88.1	11.19
	<u>100.0</u>		<u>782.1</u>	<u>100.0</u>

## Exhaust Gas

	% Vol.			% Wt.
$CO$ —	0	$\times 14 =$	0	0
$CO_2$ —	7.05	$\times 22 =$	155.1	2.56
$O$ —	5.45	$\times 16 =$	87.2	6.49
$N$ —	87.00	$\times 14 =$	1218.0	82.95
	<u>100.0</u>		<u>1460.3</u>	<u>100.0</u>





# Properties of Gases.

## Philadelphia Illuminating Gas

$C_p$	$C_v$
$CO_2 - 6.7 \times .217 = 1.453$	$6.7 \times .1535 = 1.03$
$CO - 29.3 \times .2479 = 7.260$	$29.3 \times .175 = 5.15$
$O - 1.22 \times .2175 = .265$	$1.22 \times .155 = .189$
$H - 4.05 \times 3.409 = 13.800$	$4.05 \times 2.412 = 9.750$
$CH_4 - 37.65 \times .593 = 22.350$	$37.65 \times .467 = 17.55$
$C_2H_4 - 9.89 \times .404 = 3.990$	$9.89 \times .352 = 3.28$
$N - 11.19 \times .2438 = 2.730$	$11.19 \times .173 = 1.935$
<u>51.848</u>	<u>38.864</u>

$$R_g (\text{1 lb gas}) = 51.848 - 38.864 = 12.984 \text{ B.T.U.}$$

$$= 101.2 \text{ foot pounds.}$$



# Exhaust Gas

$C_p$	$C_v$
$CO_2 - 10.56 \times .217 = 2.285$	$10.56 \times .1535 = 1.621$
$O - 6.49 \times .2175 = 1.410$	$6.49 \times .1535 = 1.006$
$N - 82.95 \times .2438 = \underline{20.250}$	$82.95 \times .173 = \underline{14.350}$
$23.945$	$16.977$

$$R_e \text{ (per lb of gas)} = 23.945 - 16.977 = .06968 \text{ B.T.U.}$$

$$= 54.211 \text{ foot-lbs.}$$

Gas for ignition in cubic ft per hour. Found by dividing the number of cu. ft. by the time in minutes taken to pass through, multiply by 60 and divide by calibration of the meter.

$$\text{Gas-ignition} = \frac{5.5 \times 60}{62.5 \times 1.001} = 5.28 \text{ cu ft}$$



Same for gas for combustion

$$\text{Gas} \quad \frac{25 \times 60}{64.15 \times 1.177} = 19.8 \text{ cu. ft. per hour}$$

Calorific Value of Gas.

$$\text{CO} \quad \text{---} \quad 4300 \times .293 = 1259.$$

$$\text{CH}_4 \quad \text{---} \quad 23500 \times .3765 = 8847.75$$

$$\text{C}_2\text{H}_4 \quad \text{---} \quad 21400 \times .0989 = 2116.46$$

$$\text{H} \quad \text{---} \quad 52500 \times .0405 = \underline{2126.25}$$

$$\text{Value per lb. gas} = 14349.46 \text{ B.T.U.}$$

Ratio of air to gas by weight.  
Find the ratio of gas to carbon  
in the fresh gas and multiply  
by the per cent of carbon in  
exhaust gas. The result is the  
per cent of gas supplied to form  
the exhaust gas. The remainder  
of exhaust gas is air.





11

gas in combination of gas and air.

Fresh Gas % C

$$C \text{ in } CO_2 = 1.7 \times 6.7 = 11.3$$

$$C \text{ in } CO = 2.1273 = 12.57$$

$$C \text{ in } C_2H_4 = \frac{2.4}{2} \times 7.19 = 8.48$$

$$C \text{ in } C_4H_4 = \frac{1.2}{1.6} \times 39.65 = 28.23$$

$$\text{Total C} = 51.13$$

Exhaust Gas, % C

$$C \text{ in } CO_2 = 4.2 \times 2.56 = 10.75 \quad \text{Total C}$$

$$\% \text{ Gas} = \frac{100}{51.13} \times 2.88 = 5.64\%$$

$$\% \text{ air supply} = 100 - 5.64 = 94.36$$

$$\begin{aligned} \therefore \text{Lbs of air per lb of gas} &= \frac{94.36}{5.64} \\ &= 16.75 \text{ lbs} \end{aligned}$$

Specific Volume of gas in  
main =  $\frac{RT}{P}$

P bar. pres. + gauge pres. - vapor pres.



$$\text{Bar. pres.} = 30.06 \times .4888 = 14.69 \text{ lbs per sq. in.}$$

$$\text{gauge pres.} = 2.4 \times .0361 = .0866 \text{ lbs per sq. in.}$$

Assume gas is saturated.

Vapor pressure saturated at  $85^{\circ}\text{F}$ .

$$= .591 \text{ lbs per sq. in.}$$

$$\therefore P = 14.69 + .0866 - .591 = 14.1856 \text{ lbs per sq. in.}$$

$$\therefore \text{Specific Vol} = \frac{101.2 \times (460.7 + 85)}{14.1856 \times 144}$$

$$= 26.98 \text{ cu ft}$$

$$\text{Vol. gas per explosion} = \frac{\text{cu. ft. per hour}}{60 \times \text{explos. per min.}}$$

$$= \frac{19.8}{60 \times 141.1} = 0.00233876 \text{ cu ft}$$

Weight of gas per explosion

$$= \frac{\text{vol. per explosion} \times .00233876}{\text{specific volume} \quad 26.98}$$

$$= .000086685 \text{ lbs}$$



Wt. of air per explosion - wt. of gas per  
 expls.  $\times$  ratio air to gas -  $16.75 \times 0.0008665$   
 $= .00145197 \text{ lbs.}$

Total air per hour =  $.00145197 \times 14.11 \times 60$   
 $= 12.2915 \text{ lbs.}$

Volume of air per hour =  $\frac{MRT}{P}$

$P$  = Bar. Pres - vapor pressure

$T = 86.23$       Saturation = 71%

Bar pressure = 14.72 lbs per sq. in.

Pressure assuming saturation = .61 lbs

$\therefore$  vapor pressure =  $.61 \times .71 = .43 \text{ lbs per sq. in.}$

$\therefore P = 14.72 - .43 = 14.29$

$\therefore V = \frac{12.29 \times .00145197 \times (86.23 + 460.7)}{14.21 \times 144}$

$= 174.375 \text{ cu. ft. per hour}$

Volume of air used only when  
 explosions. When there  
 are explosions, only air is





drawn in. Assuming the pressure on gas and air is same and that cylinder volume is sum of the volumes of the gas and air we get formula (1). &

$$M_a' = 12.29 \times \frac{141.1}{\frac{318.4}{2}} - \frac{18.1 \times 101.2 \times .000086685 \times 141.1 \times 60}{\frac{318.4}{2} \times 53.37}$$

$$= 10.893 - .15821 = 10.735 \text{ lbs per hr.}$$

$$\therefore \text{Lbs per explosion} = \frac{10.735}{60 \times 141.1} = .001268 \text{ lbs}$$

$$\begin{aligned} \text{Volume of air for explosions per hour} \\ = \text{total vol of air} \times \frac{\text{wt. air for explosions}}{\text{wt of total air}} \end{aligned}$$

$$= 174.375 \times \frac{10.735}{12.29} = 152.31 \text{ cu. ft.}$$

$$\text{Volume per explosion} = \frac{152.31}{60 \times 141.1}$$

$$= .017991 \text{ cu. ft.}$$



Indicated P. - See formula (14).

P. was found from the cards.

Since there were 5 cards like the first and 7 like the second, they were multiplied by these numbers respectively and divided by the sum to find mean and then by the length for the M. P.

$$\begin{aligned} \text{I. P.} &= \frac{41.98 \times 5 + 78.54 \times 9 + 141.1}{12 \times 33000} \\ &= .527 \end{aligned}$$

$$\text{since M. P.} = \frac{5 \times 24.2 + 7 \times 1.47}{12 \times 5}, \text{ scale} = 41.98$$

Brake Horse Power - See formula (15)

It is found by adding the weight of the spring balance to the indicated pull and subtracting the weight on the other end.



$$B. H. = \frac{318.4 \times 6.28 \times 4.87}{33000} = .295$$

Gas per I.H. without ignition per hour =  $\frac{19.8}{.527} = 37.57$  cu ft

Same with ignition gas =  $\frac{19.8 + 5.28}{.527}$   
 = 47.59 cu. ft.

Gas per B.H. per hour without ignition  
 =  $\frac{19.8}{.295} = 67.11$  cu ft.

Same with ignition gas =  $\frac{25.08}{.295}$   
 = 85.02 cu. ft.

Clearance.

wt. of water in cylinder = 2.912 lbs.

wt. of 15.23 cu. in. of water = .547 lbs.

total wt. of water =  $\frac{2.919 \times 15.23}{.547 \times 1728} = .047$  cu. ft.

wt. of displacement =  $\frac{32 \times .7054 \times 8\frac{1}{2}}{1728} = .0362$  cu. ft.



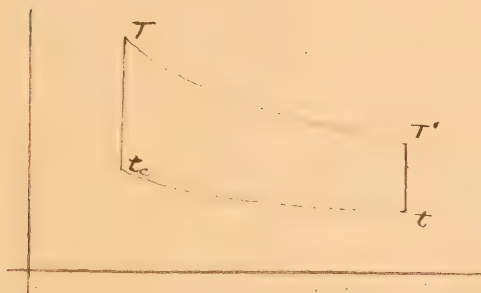


$$\text{Mean } t_c = .047 \times 2.2 = 0.1034 \text{ ft}$$

Efficiencies.

$$e = \frac{.295}{.527} = .56 \text{ from formula (20)}$$

$$E'' = \frac{.527 \times 33000}{778 \times 1.2 + 39 \times 14.1} = .1274 \text{ formula (21)}$$



$$E' = \frac{C_p(T - t_c) - C_p(T' - t)}{C_p(T - t_c)}$$

Since both curves are adiabatic, and pass through the same volume change

$$\frac{T'}{T} = \frac{t}{t_c}$$

From this we have  $\frac{T' - t}{T - t_c} = \frac{T'}{T} = \frac{t}{t_c}$ . Then

$$E' = 1 - \frac{T'}{T} = 1 - \frac{t}{t_c}.$$

On page 24, formula 21,  $E'$  is expressed in terms of the volumes by replacing



the temperatures by their equivalents in volumes.

$$\text{Volume of piston displacement} = \frac{3^2 \times .7854 \times 5^2}{1728} \\ = .0204 \text{ cu. ft.} = v_4$$

$$\text{Total volume} = .0204 + .0108 = .0312 = v_3$$

$$E_1 = 1 - \left( \frac{.0108}{.0312} \right)^{4/3} = 1 - .647 = .353$$

$$E_2 = \frac{.1274}{.353} = .361 \quad \text{formula (23).}$$

Heat Cutting Engine.

$$H_c = 14349.46 \times .000086685 \times 141.1 = 175.57 \text{ B.T.U.}$$

per min. formula (21)

$$H_a = .2375 \times 16.75 \times .000086685 \times 141.1 \times (86.23 - 32) \\ = 2.6387 \text{ B.T.U.} \quad \text{formula (3).}$$

Wet here in air.

wt. of vapor in 1 cu. ft. of saturated air at 86.23°

$$F = W_{\text{air}} = .001914 \text{ lbs.}$$

wt. when humidity = 71% or h. =  $h_{\text{air}} = W_{\text{air}}$

$$= .71 \times .001914 = .001359 \text{ lbs.}$$



Vapor press. at  $86.23$  when saturated =  $P_{am} =$   
 $.6107$  in. Hg

$P_{am}' =$  press at  $71\%$  humidity =  $.71 \times .6107 = 437.1/100$

$T_{am}' =$  corresponding temp. to  $P_{am}' = 75.63$ .

When the air is not saturated the vapor is superheated, and therefore the heat brought in in the moisture is equal to the heat of the liquid, the heat of vaporization and the heat of superheat. By formula (4)

$$H_{am} = .001359 [43.75 + 1061.3 + .48(86.23 - 75.63)]$$
$$\times \frac{174.375}{60} = 4.3844 \text{ B.T.U. per min.}$$

$$H_g = .5785 \times .000086685 \times 141.1 \times (85 - 32) =$$
$$.33612 \text{ B.T.U. per min. formula (5)}$$

Since the fresh gas is saturated with moisture, the heat brought in in the moisture is equal to the heat of the liquid and the heat of vaporization. By formula (6)

$$H_{gm} = .001813 \times 1107.9 \times \frac{19.8}{60} = .66284$$





.001813 lb. is the mass of moisture  
in 1 cu. ft. of gas at the temperature  
of the gas  $85^{\circ}\text{F}$ . when saturated.

### Heat Leaving Engine.

The indicated work is here ex-  
pressed in B. T. U. by formula (10)  
$$H_i = \frac{5.27 \times 33000}{778} = 22.353 \text{ B. T. U. per min.}$$

The heat leaving in the jacket water  
as expressed by formula (9) is  
the mass of water multiplied by  
the difference between the heat of  
the liquid at entrance and exit.

$$H_j = \frac{261.75}{60} \times 26.1 = 113.861 \text{ B. T. U.}$$

$$\begin{aligned} H_e &= .23445 \times (427.4 - 32) \times (.20456 + .01223) \\ &= 20.554 \text{ B. T. U. By formula (7)} \end{aligned}$$



Wetness in exhaust air

$$H \text{ in } 1 \text{ lb. fresh gas (free)} = .0405 \text{ lb.}$$

$$H \text{ in } C_2H_4 = \frac{4}{28} \times .0989 = .0141 "$$

$$H \text{ in } C_2H_6 = \frac{4}{16} \times .3765 = .0941 "$$

$$\text{Total } H \text{ in 1 lb. of gas} = .1487 "$$

$$\text{wt. of } H_2O \text{ formed from } H = 4 \times .1487 = 1.3353 \text{ lb.}$$

$$\text{amt. of gas per min.} = .01223 \text{ lb.}$$

$$H_2O \text{ formed per min.} = .01223 \times 1.3388 = .01637 \text{ lb.}$$

$$H_2O \text{ in air per min.} = .00395 "$$

$$" \quad " \quad \text{gas} \quad " \quad " = .00060 "$$

$$\text{Total moisture} = .02092 "$$

By formula (12) we obtain pressure of vapor, and from latter the corresponding temperature may be found.

$$P_{\text{v}} = \frac{14.72}{1 + \frac{.21704 \times 54.211}{.02092 \times 85.732}} = 1.95 \text{ lb. } \sigma "$$

$$\text{Corresponding temp.} = 125.5^\circ F$$



From a similar formula to that used in finding heat in weight in moisture of air we have by formula (8)

$$H_{mo} = .02092 [93.5 + 1026.7 + H(427.4 - 125.9)]$$

$$= 26.466 \text{ B. T. U.}$$

Heat Balance.

Entering

	per min.	per 100 B. T. U.
Combustion	175.57000	95.624
Air	2.63870	1.438
Moist. of Air	4.38440	2.389
Gas	.33612	.183
Moist. of Gas	.66284	.361
	<hr/> 183.53206	<hr/> 100.000





# Leaving.

	per min	per 15 H.T.U.
I. H. P.	22.353	12.174
Condenser	113.101	62.038
Ex. Gas.	20.554	11.200
Flue Gas Ex. Gas	26.466	14.420
Radiation	<u>.299</u>	<u>.163</u>
	183.532	100.000

The heat lost by radiation is the amount of heat by which the heat leaving the engine is less than the heat entering.

$$R_r = 183.532 - 183.233 = .299 \text{ H.T.U.}$$



# Result of Test

Day 1 1888

1.	Duration of test in minutes	60
2.	Diameter of cylinder in inches	3
3.	Length of stroke in inches	5
4.	Circumference of flywheel in feet	6.28
5.	Atmospheric pressure (barometer) inches	30.36
6.	" " " lbs. per sq. in.	14.69
7.	Pressure in gas main in inches of water	2.4
8.	max. pressure in cylinder above atmosphere in lbs. per sq. in.	114
9.	Mean effective pressure in lbs. per sq. in.	41.98
10.	Mean temperature of air	86.23
11.	" " " fresh gas	85
12.	" " " exhaust air	457.4
13.	" " " entering jacket water	80.2
14.	" " " leaving " "	106.4
15.	" effective pull on brake in lbs.	487
16.	Revolutions per minute	318.4
17.	Explosions per minute	141.1



18.	Indicated horse power	.527
19.	Brake horse power	.295
20.	Gas per hour without ignition (cu. ft.)	19.8
21.	" " " for " (" ")	5.28
22.	Total gas per hour (cu. ft.)	25.08
23.	Wt. of gas per explosion (lbs)	.0008668
24.	Vol. of gas per explosion (cu. ft.)	.00233876
24a.	Calorific value of gas per lb. in B.T.U.	14349.5
25.	" " " per explosion "	1.2439
26.	Gas per I.H.P. per hr. without ignition (cu. ft.)	37.57
27.	" " " " " with " (" ")	47.59
28.	" " B.H.P. " " without " (" ")	67.11
29.	" " " " " with " (" ")	85.06
30.	Wt. of air per lb. of gas.	16.75
31.	Wt. of air per explosion (lbs)	.00145797
32.	Vol. of air per explosion (cu. ft.)	.017991
33.	Vol. of air per hr. for explosion (cu. ft.)	152.31
34.	Total air per hour (cu. ft.)	174.375
35.	Total air per hour (lbs)	1229.15
36.	respe efficiency	.253





37.	Actual efficiency	.1274
38.	Ratio of actual to type	.361
39.	Mechanical efficiency	.56





Equation of  
Curvature  
Curve

The general  
equation of the  
curve is

$p^2 = K$   
by the method  
of least squares  
the value of the  
coefficient  $K$   
may be obtained.

The equation  
 $p^2 = K$  is  
expressed in  
the following  
form -  
 $\log p^2 = \log K$   
A number of



equidistant points was selected on the abscissa and the pressure and volume for each point measured on the curve. The logarithms of these values were substituted in the equation given above.

Then the coefficient of  $u$  was taken and used as a multiplier in each equation. This a second set of equations were obtained. Each set were added and two equations containing two unknowns -  $K$  and  $u$  - were obtained. These were solved for  $u$ .

Then the curve  $p_v = K$  was drawn. According to the value of  $u$  the expansion curve should fall above or below the curve  $p_v = K$ . If  $u$  is less





than one the expansion curve should fall above  $p_0 = K$ . If greater than one the curve  $p_0 u = K$  should fall below the curve  $p_0 = K$ .

Solving for  $u$  as described above we obtained a value

$$u = 1.154.$$







3 1198 03073 4029



N/1198/03073/4029X

ST